



Animal Rendering Wastewater Treatment Process Utilizing Zeolite Based Ammonium Capture

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Abstract

Animal Rendering Condensate Wastewater (RCWW) produced by slaughterhouses is rich with ammonia, oils, phosphorus, and other components. When RCWW is dumped into a body of water, algal blooms and dead zones are likely to form and cause significant environmental damage. This project presents an approach of utilizing zeolite ion exchange for ammonium removal in the downstream processing stages of the RCWW treatment process and makes a comparison to other common methods such as distillation and reverse osmosis. Aspen was used to simulate the zeolite exchange and distillation, and reverse osmosis data was used to compare. The zeolite column is shown to be the cheapest by about \$25k per year compared to the next best (rev. osmosis)

Introduction and Background

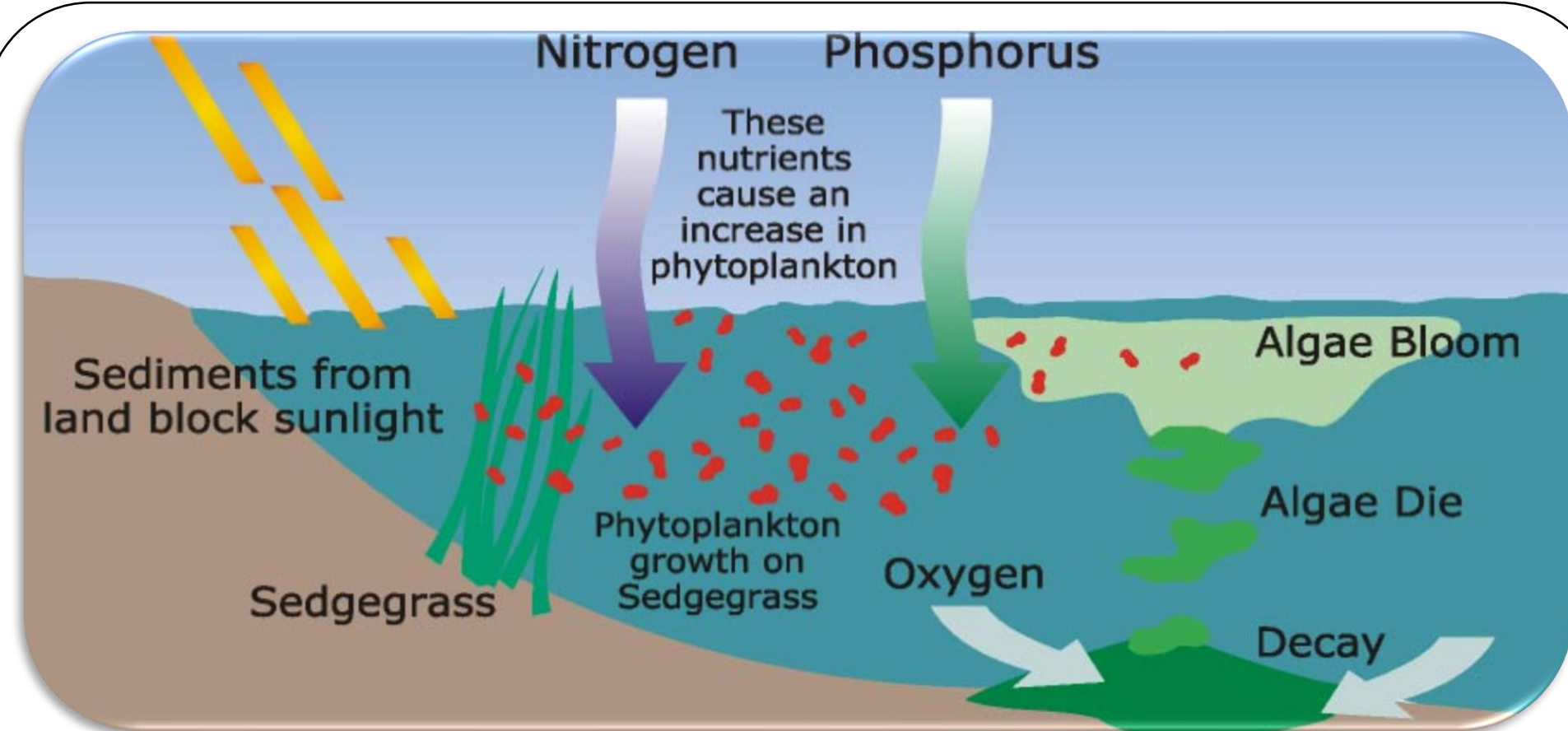


Figure 1: Eutrophication Process in freshwater¹

- Illegal disposal of RCWW into the Chesapeake Bay has caused widespread eutrophication².
- RCWW contains high levels of pollutants (COD > 10,000 mg/L, Ammonia > 850 mg/L)³

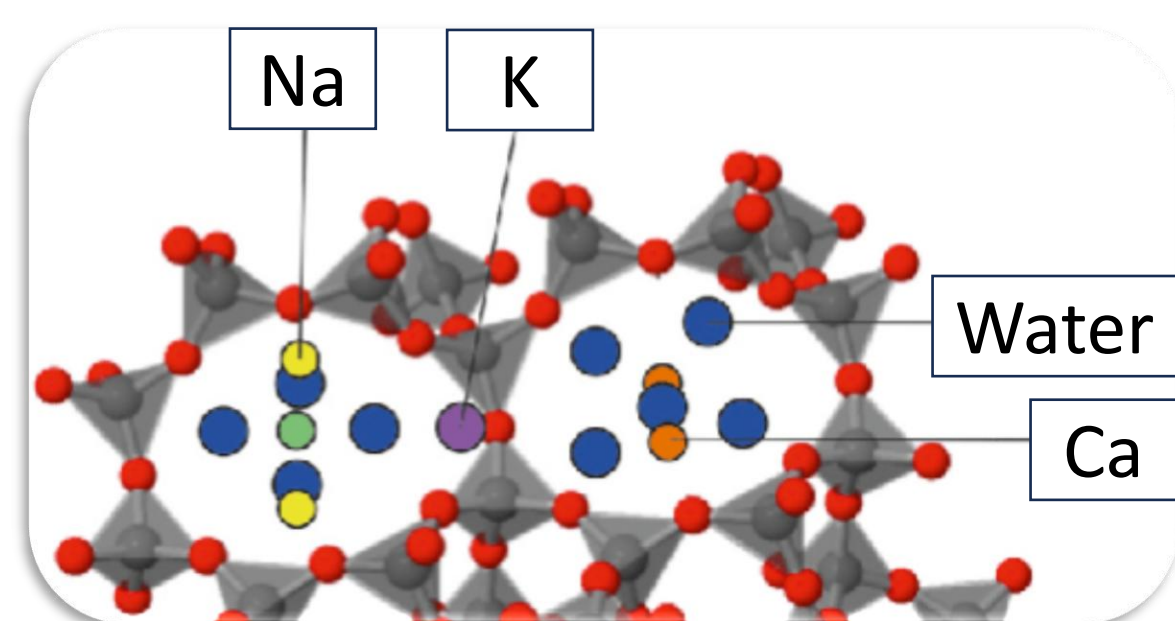


Figure 2: Clinoptilolite (zeolite) molecular structure and ion formation (Na, K, Ca, etc.) within its structure⁴

- Clinoptilolite is a zeolite that has a high affinity for ammonium compared to other ions
- Columns can be regenerated with concentrated salt brines, and are cheap to maintain

Methodology

- Ammonia Separation Processes simulated utilizing Aspen Adsorption
- Modeled using equations: Convection Dispersion Model, Solid Film Model, and Stoichiometric Equilibrium Isotherm^{5,6}
- Specifications: constant density/velocity, no pressure drop, isothermal, fixed MTC^{5,6}
- Column performs ion exchange within the zeolites then NH₃ elution is driven with elevated levels of NaCl

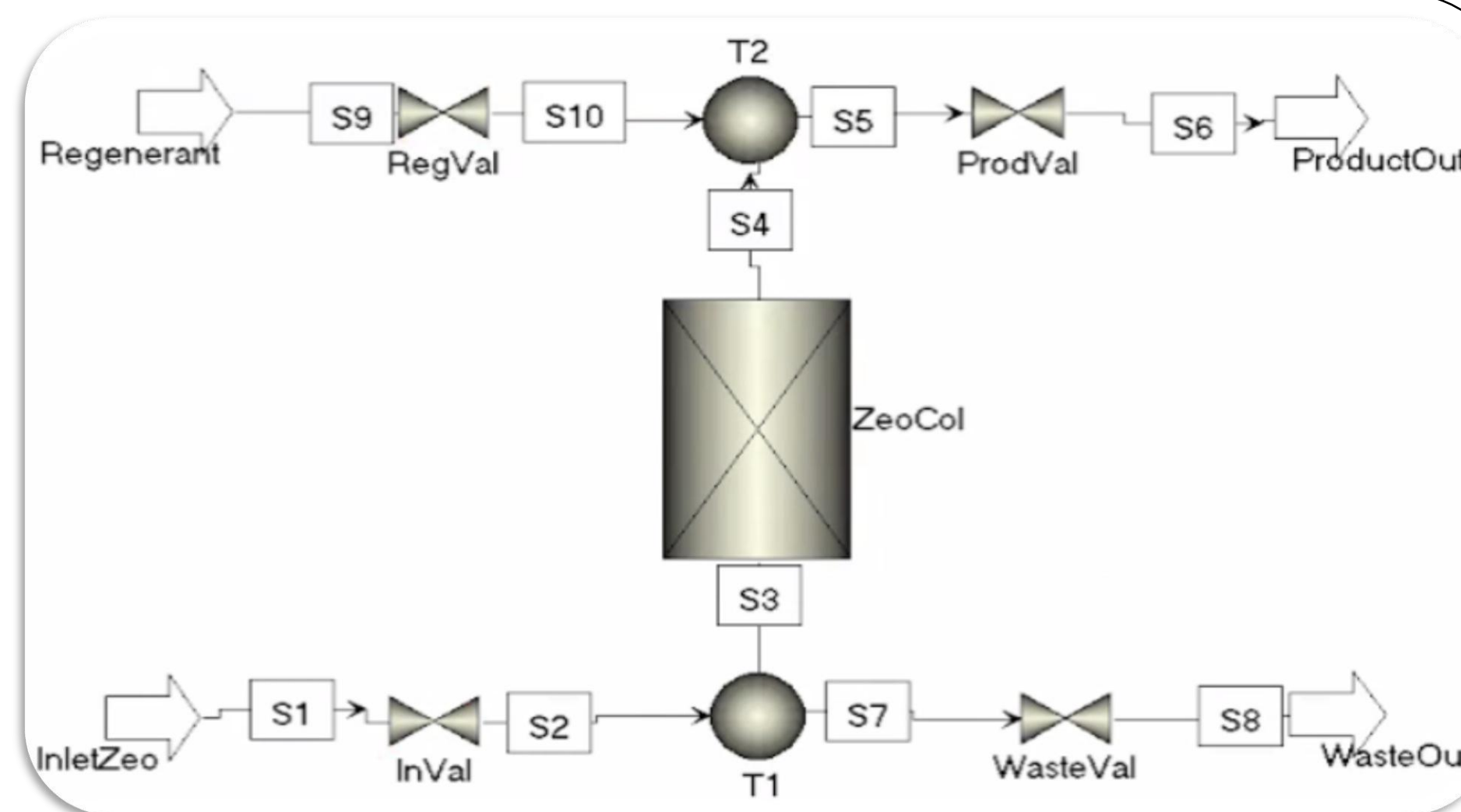


Figure 3: Aspen Adsorption Zeolite PFD

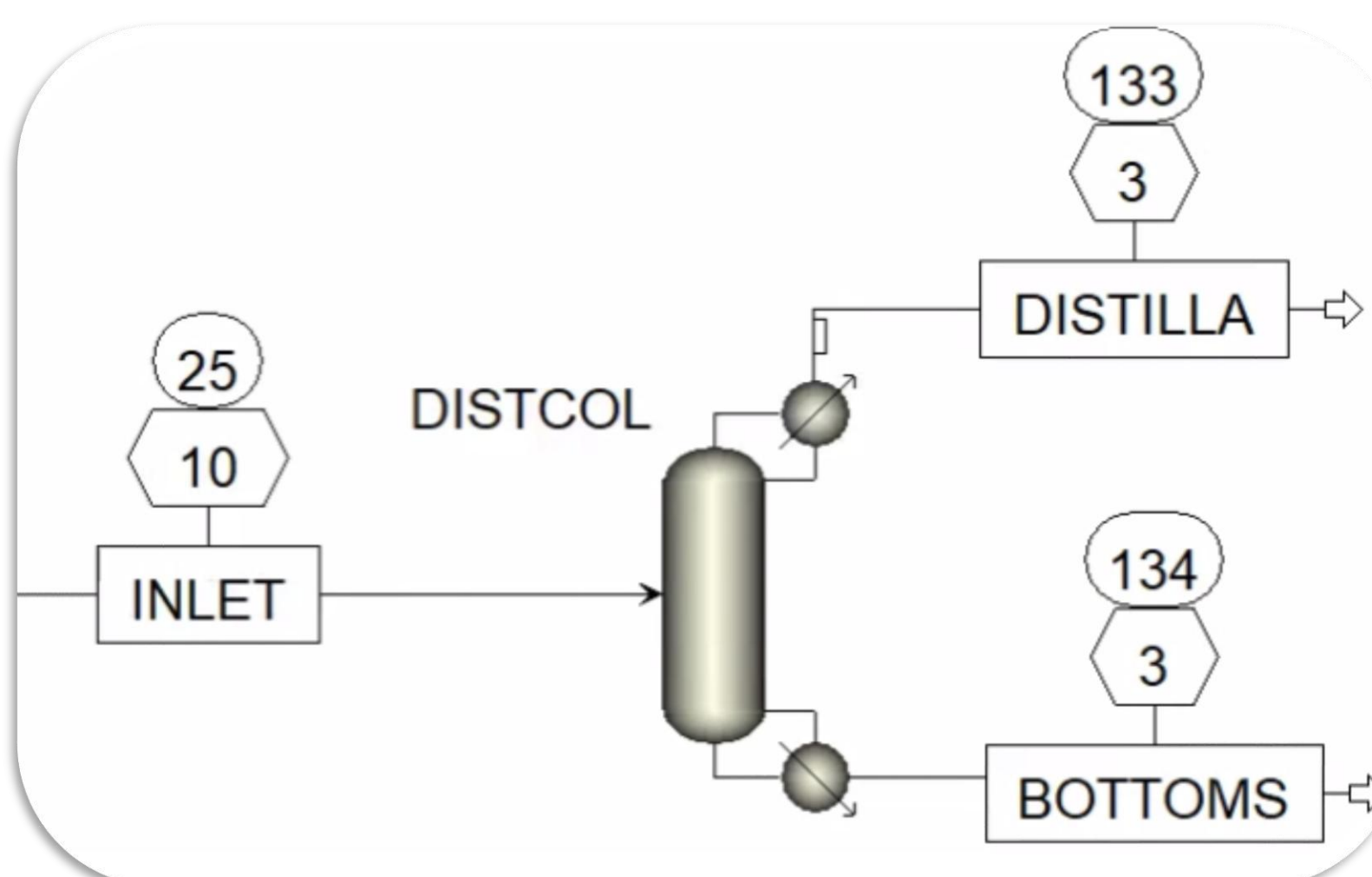


Figure 4: Aspen Plus RadFrac model for distillation

- Aspen Plus RADFRAC block enables regeneration of the zeolite column by separating ammonia from a brine regenerant stream
- Added enough energy to reboiler to result in an effluent containing low levels of NH₃ at 1 mg/L
- Sensitivity analyses on distillate-to-feed and reflux ratios identified optimal operating ranges (D:F = 0.1–0.3, Reflux = 0.4–0.6) to maximize NH₃ purity while minimizing energy usage

Zeolite Column Simulation Results

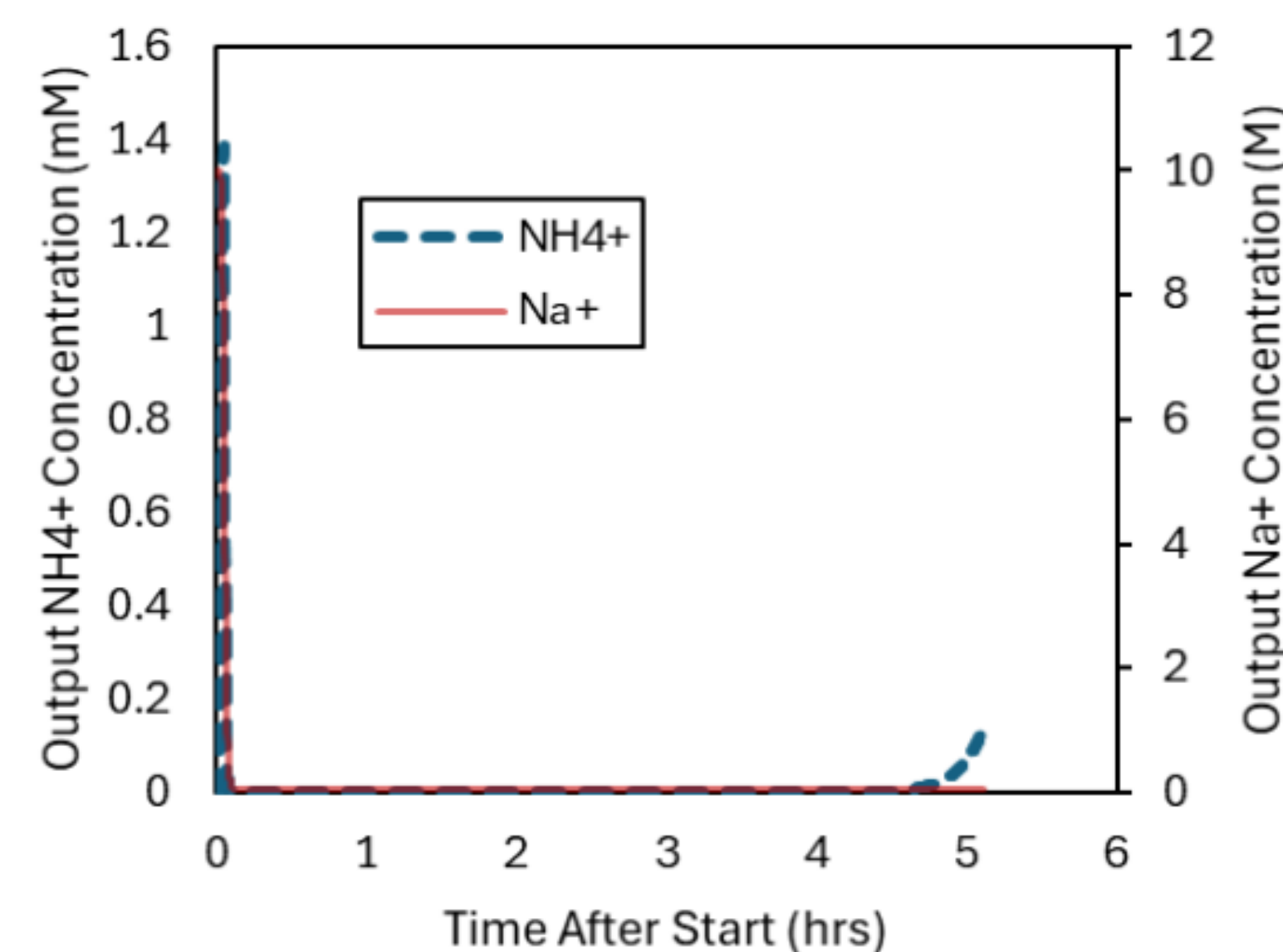


Figure 5: Product stream output concentration over 5-hr period.

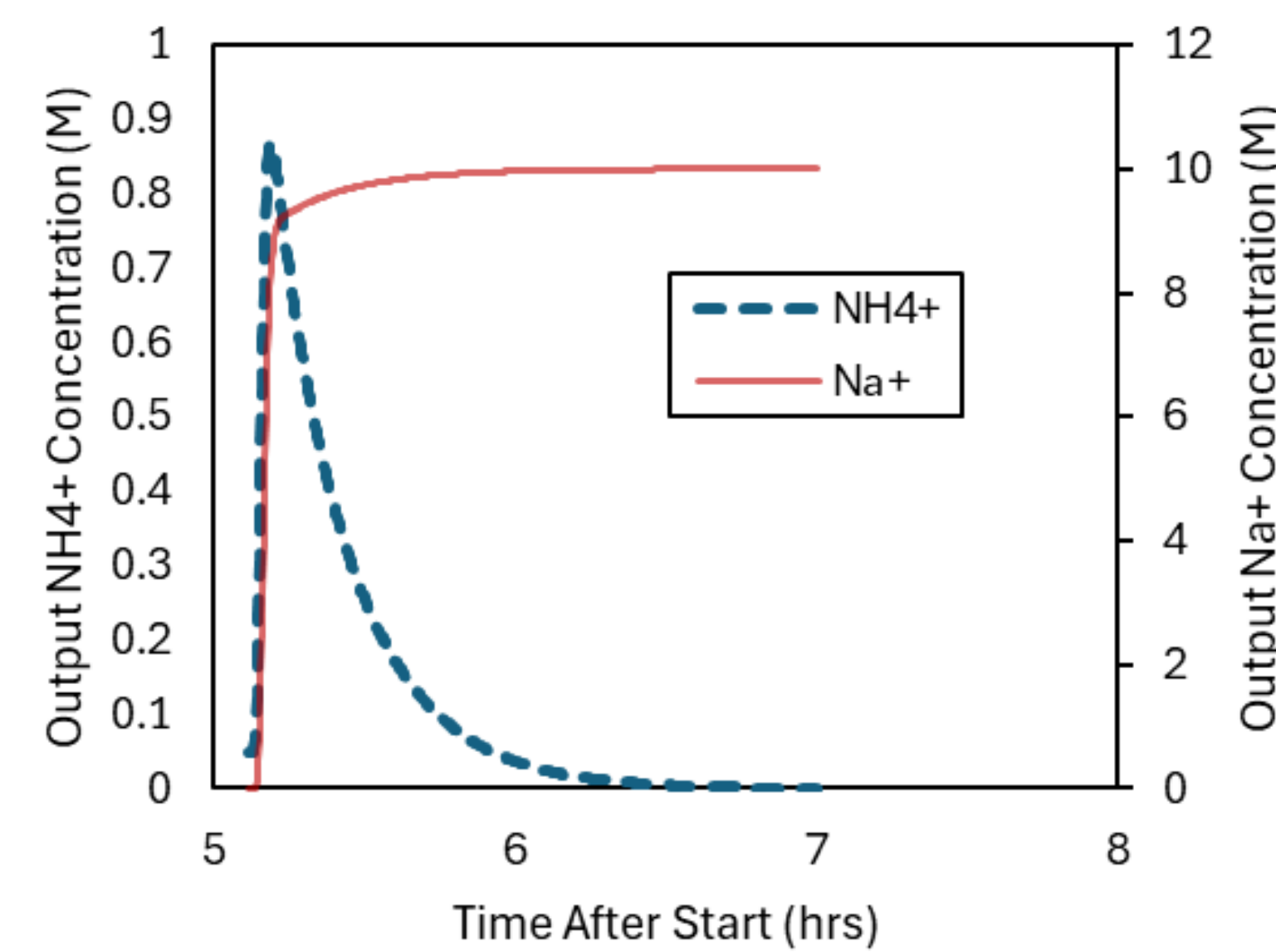


Figure 6: Backwash stream utilizing salt brine regenerant (10M NaCl) after column saturation.

- Shows a 5-hour adsorption time followed by a 2-hour regeneration time
- During regeneration high concentration of NaCl displaces NH₄⁺ from column via another ion exchange and NH₄⁺ sharply increases
- Output NH₄⁺ limit for the product stream set to 1 mg/L
- Optimization of temperature, grain size, and pH was completed

Economic Analysis

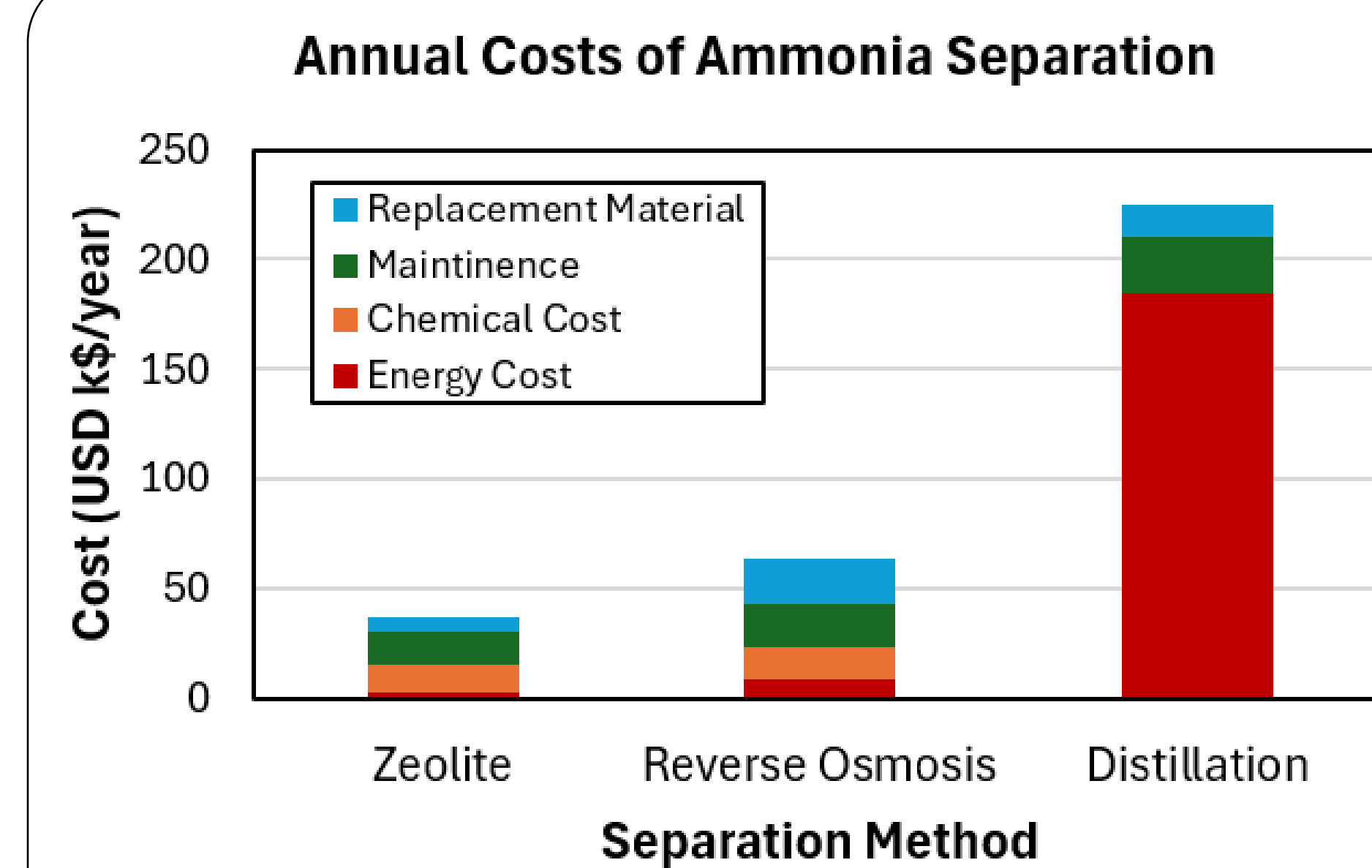


Figure 7: Economic analysis of annual cost of each method

Conclusions/Recommendations

- The system with zeolite treatment provides a more cost-effective removal of ammonia compared to the competitors
- The zeolite column operates most effectively and cheapest at a neutral pH with grain sizes in the 1mm range, and at warmer temperatures 25–35 C
- Other configurations could be optimal depending on the variation of RCWW content. More rigorous separation methods might be needed

Future Work

- Simulating zeolite regeneration for multiple cycles with updated component concentrations
- Measuring the accumulation of ammonia in the regeneration stream when recycled, and analyzing when the zeolite effectiveness starts to drop off

References

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