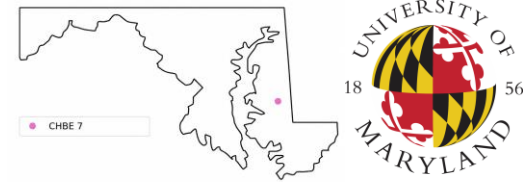


Team 7: Green Ammonia in Maryland (GAM)

Kenny Nguyen, Nathaniel Miller, Aman Sagmanligil, Alessandro Ramirez

Chemical & Biomolecular Engineering



Background:

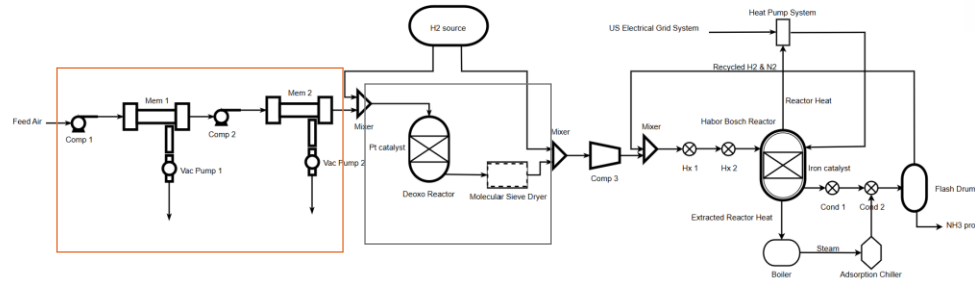
Maryland currently relies on **out-of-state, fossil-fuel-based** ammonia production, which generates significant greenhouse gas emissions despite **steady fertilizer demand**, while regional wind and solar resources are **growing but remain underused** for industrial manufacturing. The purpose of this process is to **modernize** the Haber-Bosch ammonia production with these technological advances

Goals:

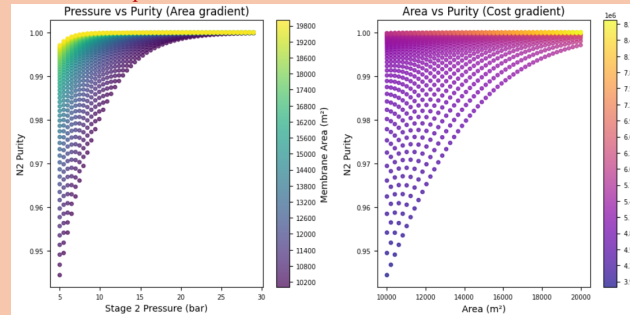
- Ammonia Requirement per Acre = 76.66 kg/yr
- Harvested Farmland in Maryland 2022: 1,274,673 acres
- Total Ammonia needs of Maryland: **97,713 tons/yr**
- Ammonia Purity: 99%
- MAX CO₂ Emissions: 25,000 tons/yr
- IRR: 5-10%

Stakeholders:

Stakeholder	Concerns	Needs	Wants
Investors	Not Losing Money	Rate of Return > Cost of Capital	10% Rate of Return
Customers	Product Purity, Quantity	High Product Purity	Consistent Large Supply of Ammonia
Operating Engineers	Safety and Operability	Design Within OSHA Regulations	Minimal Risk and Ease of Use.
Environmental Organizations	Environmental Impacts of Plant	Environmental Impact Within Regulations	Sustainable, Low Footprint Design
General Populace	Pollution	Minimal Impact to Local Environment	No Change to Daily Life



Membrane Separators: 11632.65 m² membrane



Post Oxygen Removal:

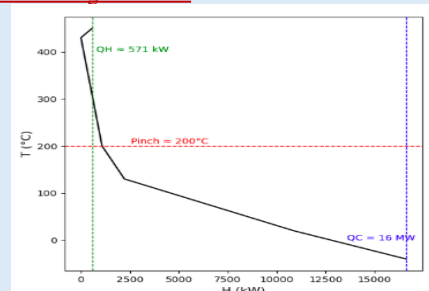
N₂ : 99.998527261 %
 Ar : 0.0004208669 %
 CO₂ : 0.0000002854 %
 O₂ : 0.0000000000 %
 H₂ : 0.0009515677 %
 H₂O : 0.0001000189 %

Flow rate: **93.00 mol/s**
 Temperature: 300.79 K
 Pressure: **28.01 bar**

Haber-Bosch Reactor:

	Reactor	Condensers	HXs	Compressor
Temperature (°C)	450	450 → -20	94 → 450	37 → 304
Pressure (bar)	150	150	150	28 → 150
Heat/Work Duty (kW)	-9978.8	-16256.1	10195.7	2959.2

Heat Exchange Network:



Economic Analysis:

Total Cost of System: \$160.6 million

Reactor: \$19.9 million
 Nitrogen Separator: \$2 million
 Storage Tanks: \$35.2 million
 Compressor: \$7.5 million
 Heat Exchangers: \$700k
 Heat Pump: \$2.8 million
 Absorption Chiller System: \$4.4 million
 Piping and Infrastructure: \$58.4 million
 OSBL investment: \$29.2 million

Operating Cost: \$50.8 million/yr

Nitrogen Separator: \$6.3 million/yr
 Hydrogen: \$35.1 million/yr @ \$2/kg
 Electricity: \$3.1 million/yr
 Personnel: \$469k/yr
 Property Tax & Insurance: \$1.5 million/yr
 Rent of Land: \$2 million/yr

Earnings:

Revenue: \$77.5 million/yr @ \$0.78/kg
Post-Tax Profit: \$18.9 mil/yr @ 29.25% tax
 Payback Period: 8.5 years

Major Findings:

- Ammonia Production: **99,319 metric tons/yr** at 99.5% purity
- Only **338 metric tons CO₂** emissions per year.
- IRR: **10% over 20 years**
- Heat Delivered via Heat Pump: **571 kW**

Sustainability Assessment:

- 489 metric tons CO₂ emissions saved from heating, and 614 metric tons from removing the need for ammonia shipping. The equivalent of **5.46 tractor trailers!**
- 84566.7 m³ water saved. Equivalent of **33.8 Olympic swimming pools!**

Conclusion/Recommendation:

- Membrane Separation is **feasible** for industrial N₂ separation but suffers diminishing returns with scale up
- In the future, with green hydrogen production and renewable energy scale up, this system will become both more **economically and environmentally viable**.
- Explore possible use cases for system waste heat
- Perform cost analysis of liquid H₂ storage over gaseous H₂

Reference:

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